Amendments to the Specification:

The paragraph beginning on page 4, line 10 has been amended as follows:

Effects of prevention of polymerization have not been fully solved by the above methods, and it is desired to distill the above-mentioned solution of polymerizable (meth)acrylic acid ~~solutions of polymerizable~~ for a long period of time.

The paragraph beginning on page 5, line 14 has been amended as follows:

(i) A (meth)acrylic acid solution from a collection column for (meth)acrylic acid is generally exposed to air for the time being, then fed to a distillation column or tower set at a prescribed temperature. A temperature difference is present between (meth)acrylic acid solution as the raw material and the entrance place, at which the raw material liquid enters, in the distillation column. When the temperature difference is high, there ~~are~~ is occurred partial condensation or drift flow of the (meth)acrylic acid solution in the column, and polymerization is liable to occur.

The paragraph beginning on page 7, line 13 has been amended as follows:

Propylene and/or acrolein are allowed to partially oxidize with a molecular oxygen-containing gas, such as oxygen and air or the like, in the presence of a known catalyst. Generally, oxidation reaction is performed in a two-step procedure. The first catalyst is capable of oxidizing a raw material gas containing propylene to form mainly acrolein, and then the second catalyst is capable of oxidizing a raw material gas containing the resultant acrolein to form mainly acrylic acid. The first catalyst may contain complex oxides of iron, molybdenum and bismuth, and the second catalyst may contain vanadium at essential component. The oxidation reaction may be performed in the temperature range of 250°C to 380°C. ~~See JP-A-11-130 722, which is incorporated herein by reference in its entirety.~~

The paragraph beginning on page 10, line 14 has been amended as follows:

In the present invention, it is ~~prefer~~ preferable to adjust the temperature difference within 30° C together with to make the fluctuation range of temperature (T0) of the raw material liquid smaller. To put it concretely, it may adjust the fluctuation range to fulfill the following condition (2).

The paragraph beginning on page 11, line 7 has been amended as follows:

In addition to the above, it is preferred to make the temperature of raw material liquid (T0) smaller than the bottom temperature of the distillation column (T2). This is because when the raw material liquid having a ~~high~~ higher temperature than the bottom temperature is fed to the column, a harder environment than the essential maximum temperature to be operated (the bottom temperature) is formed within the column, and the effects of the present invention cannot be exhibited to the highest possible extent.

The paragraph beginning on page 13, line 22 has been amended as follows:

Lastly, the present invention will be explained in more detail with reference to a distillation column for separating high boiling point materials. Here, the high boiling point material means a compound having a higher boiling point temperature than that of ~~a~~ the purified material, such as maleic acid in the case of acrylic acid. Separating high boiling point materials is usually performed for the raw material liquid containing acrylic acid, and preferably performed after the separation of acetic acid from the raw material liquid and/or the distillation for separating aldehydes in the column. The distillation condition (steady state) in the distillation column is usually as follows: